

# The Production of the Matrix Component of the Fluid Catalytic Cracking Unit from Watermelon Peel

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**Abstract:-** Fluid Catalytic Cracking is considered one of the most predominant and sophisticated contributions to the technological advancement of the petroleum industry. One of the major reasons why this is so has been the introduction of the FCC catalysts, which comprises of the crystalline zeolites, binders, matrix and fillers. The ever-increasing costs of Fluid Catalytic cracking catalysts have led researchers to develop alternative materials which can be gotten locally and have similar if not superior properties than the commercial FCC Catalyst. Over the years, there have been many significant improvements in the FCC catalysts and most of them have been focused on the zeolite. However, research over the last five decades has shown that the benefits derived from improved FCC catalyst technology- such as increased gasoline yields, improvements in catalyst attrition resistance, enhanced bottoms cracking, can be associated with advancement of the catalyst matrix technology. In this study, the matrix component of the FCC Catalyst was synthesized using watermelon peel as starting materials. The matrix was synthesized using chemical modification while varying reagent concentration and reaction time. The resultant products were evaluated using FTIR, and SEM analysis. The results prove that acid- modified activated carbon has a huge potential as matrix for the FCCU catalyst though research is still on-going.

**Keywords:** Fluid Catalytic Cracking Unit; Zeolite Y; Matrix; Palm Kernel shells; Watermelon peel.

## 1. INTRODUCTION

The fluid catalytic cracking unit (FCCU) which falls under the conversion group of the Petroleum refinery operations remains an indispensable unit operation in refineries. Due to the growing demand for high octane value gasoline, the FCCU is regarded as the heart of any petroleum refinery (Fahim et al., 2010, Mamudu et al., 2019). It converts about 40% of the heavy residues gotten from both vacuum and atmospheric distillation into lighter and more useful products with high octane value.

Although the FCCU has existed for about eight decades, it has become irreplaceable due to frequent upgrades of the catalytic process that continues to further improve product selectivity. An FCCU catalyst constitutes of four major components : the crystalline zeolites, the matrix, binder and filler. Over the years, researchers have come to discover that the ultimate performance of an FCCU catalyst largely depends on the nature and composition of the zeolite and matrix components and how all of these are integrated to

create a functional cracking system (Humphries & Wilcox 1989). Technology reviews on improved performance of FCC catalysts have been centered on advancements of zeolites in the past. In recent years, more attention is being shifted towards matrix technology innovations ( Rajagopalan, 1992).

An effective cracking system provides the ability of active alumina and a crystalline zeolite to assist in the efficient upgrading of bottom distillates into higher-quality gasoline and light cycle oil. Zeolites are hydrated alumina silicate materials made from interlinked tetrahedral of alumina (AlO<sub>4</sub>) and silica (SiO<sub>4</sub>). 130 out of 840 catalysts used in industrial applications are based on zeolites and the FCCU in petroleum refineries utilizes over 61% of these zeolite-based catalysts (Oil & Gas Journal, 2003, Elehinafe et al, 2019).

The pore distribution, acidic properties, high selectivity and thermal stability of Zeolite catalysts make them stand out amongst other non-zeolite catalysts in the FCCU due to the significant increase in gasoline yield and octane number boost. The zeolite component makes up 10-50 wt % of the catalyst and provides activity, stability, and selectivity. The matrix comprises 50-90% of the catalyst and provides desirable physical properties, as well as some catalytic activity (Leiby,1992).

Matrices have various physical and chemical properties that make them stand out as components of a fluid catalytic cracking catalyst. The matrix usually in a fluid catalytic cracking unit is considered as catalyst support which is usually silica-alumina. One of the functions of matrices is to act as a diffusion medium that allows the diffusion of hydrocarbons in and out of the catalyst particles. (Haas, 1996). It also helps to avoid over-cracking by moderating the zeolite's activity and protecting the zeolite from structural damage by facilitating heat transfer during cracking and regeneration. Another major function of the matrix is to provide the microspheres with physical strength and the attrition resistance necessary to withstand the stress of rapid circulation. It usually acts as a cracking component for gas molecules that are too large to enter the zeolite's pores. The most common matrices being used are amorphous silica, alumina and silica-alumina (Ballmoos and Hayward, 2008).

Researchers have begun to place more attention on the effect of matrices on the activity of FCC catalysts and poisoning mechanisms such as vanadium and nickel (Chen, 2005). There are various types of synthetic zeolites but a major catalyst that has continued to gain worldwide recognition is the type- Y zeolites from the faujasite family. This is so because modification and re-modification have been made on its structural framework over the past decades which have helped to upgrade its inherent physico-chemical properties- acidity, thermal stability and the evident increase in gasoline yield (Liu, 2016).

In 2003, a new catalyst called Flex-Tee was commercialized by Engelhard Corporation, the production of this new catalyst was centered around the Distributed matrix structure DSM technology. The basic concept in DSM technology was the introduction of a unique pore structure that enhances the diffusion of the feed stock molecules and the provision of highly selective pre-cracking sites (Sakashita, 2011). With respect to the matrix of an FCC catalyst, similar properties of the conventional matrix has been found in activated carbon like its resistance to attrition and large pore size which will encourage diffusion of hydrocarbon molecules (Ballmoos & Hayward, 2008).

Hence, the possibility of synthesizing pure activated carbon (matrix) from watermelon peels is studied in this work. The formulated matrix is targeted for industrial use in FCCU applications.

### 1.1 AIM AND OBJECTIVES

The aim of this study is to investigate the possibility of synthesizing matrix component of the fluid catalytic cracking catalyst from watermelon peels. This will be achieved via the following objectives;

- Chemical treatment of watermelon peel using different activating agents while varying concentration to produce activated carbon (used as a matrix in place of silica and alumina)
- Characterization of the activated carbon.

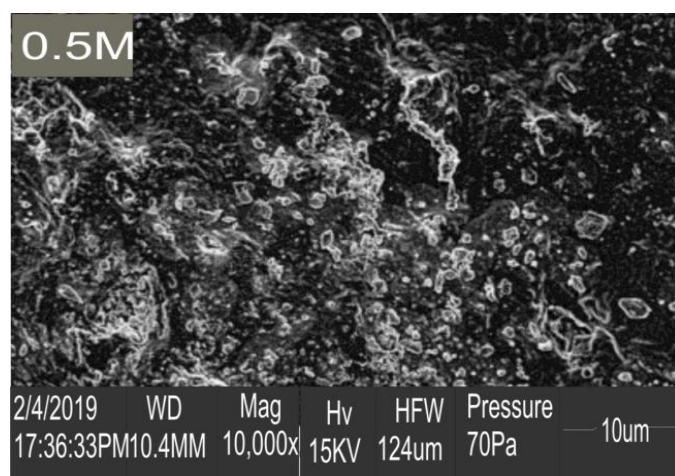


Fig 1: SEM image of (a) Synthesized AC at 10 μm

## 2.0 MATERIALS AND METHODS

### 2.2 Synthesis of FCCU Matrix

The procedure employed in the synthesis of FCC matrix was that used by Abdulkareem in the production of activated carbon. (Abdulkareem *et al*, 2014)

#### 2.2.1 Physical Treatment

The watermelon peels were gotten from the cafeteria of Covenant University. The peels were washed with distilled water to remove dirt and seeds before they were sundried for a period of 7 days to constant weight. The dried peels were then crushed to powder form using a mechanical grinder.

#### 2.2.2 Chemical Modification

12g portions of the ground watermelon peel samples were stirred and left to be soaked separately in a known weight of 1.0 M and 1.5 M, each for phosphoric acid and Zinc chloride. The impregnation ratio and time were 0.3:1 and 24 hours respectively. The activated product was then washed with warm distilled water until the distillate reached a pH of 7 to remove phosphoric acid and Zinc chloride content. The activated product was dried in an oven at a temperature of 105°C for 1 hour.

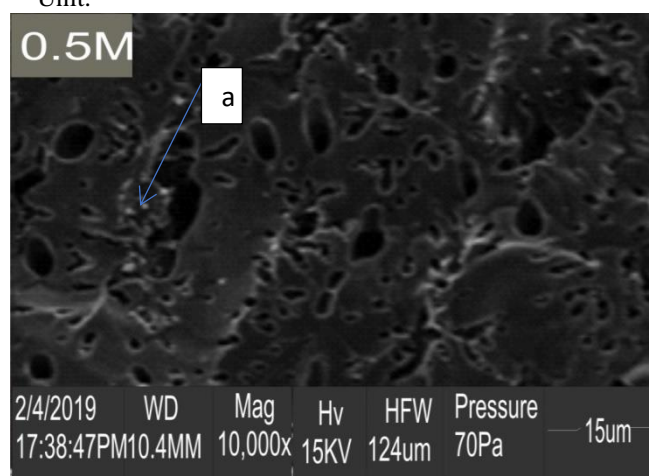
#### 2.2.3 Carbonization

In the course of the carbonization experiments, 15g of the activated samples were weighed into four different clean and pre-weighed crucibles, which were then introduced into the hot zone of a muffle furnace. The activated crushed peels were carbonized at a temperature of 300°C. The samples were held at a temperature of 60 minutes in order to establish the optimum conditions for the process. The contents were then removed from the muffle furnace after the set period and cooled in an open-air for one hour. The produced activated carbon was then characterized using SEM and FTIR.

## 3.0 RESULTS AND DISCUSSION

### 3.1 Characterization of synthesized FCCU matrix

The activated carbon produced by chemical modification of watermelon peels using Zinc chloride and phosphoric acid were characterized using SEM and FTIR to determine if it is fit to be used as a matrix in the Fluid Catalytic Cracking Unit.



### Synthesized AC at 15 μm

Fig 4.2.1a and Fig 4.2.1b give the representative image of the morphology of the activated carbon matrix. The large pores of the activated carbon are represented by the dark spaces in Fig 4.2.1b which is a property of a good matrix to ensure diffusion of molecules through the large pore openings.

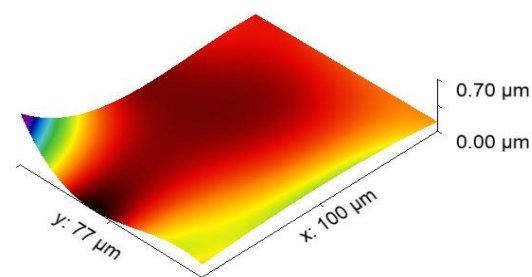


Figure 2: Structural Analysis of Synthesized Activated Carbon

Figure 2 above shows the structural effect of the chemical modification and carbonization process with a grain wise size of 147.41nm. The image shows that it is naturally compacted and evenly distributed at the centre than the edges.

### 3.3. Fourier Transform Infrared Spectroscopy Analysis

The FTIR- spectra show a band at  $3423.79\text{cm}^{-1}$  which is due to the O-H stretching of water. The band at  $1640\text{ cm}^{-1}$  has been noticed by previous researchers where C=C stretching adsorption was found to frequently occur at this region. The band observed at  $2935.76\text{ cm}^{-1}$  was found to correspond to methylene asymmetric, C - H stretching. The band given at  $1592.29\text{ cm}^{-1}$  was an indication of the presence of pyridine, C = N stretching while the band at  $1402.3\text{ cm}^{-1}$  was ascribed to azo compound, N= N stretching. Finally, the bands at  $1015$  and  $1108\text{ cm}^{-1}$  was found to be due to aliphatic C- N stretching while the band at  $683.79\text{ cm}^{-1}$  was due to P =S stretching. The FTIR shown in Figure 6 is quite similar to Figure 5 as the peaks in both spectra have a close range of values. This shows that the variation in the reagent used for chemical modification only slightly affects the absorption peaks.

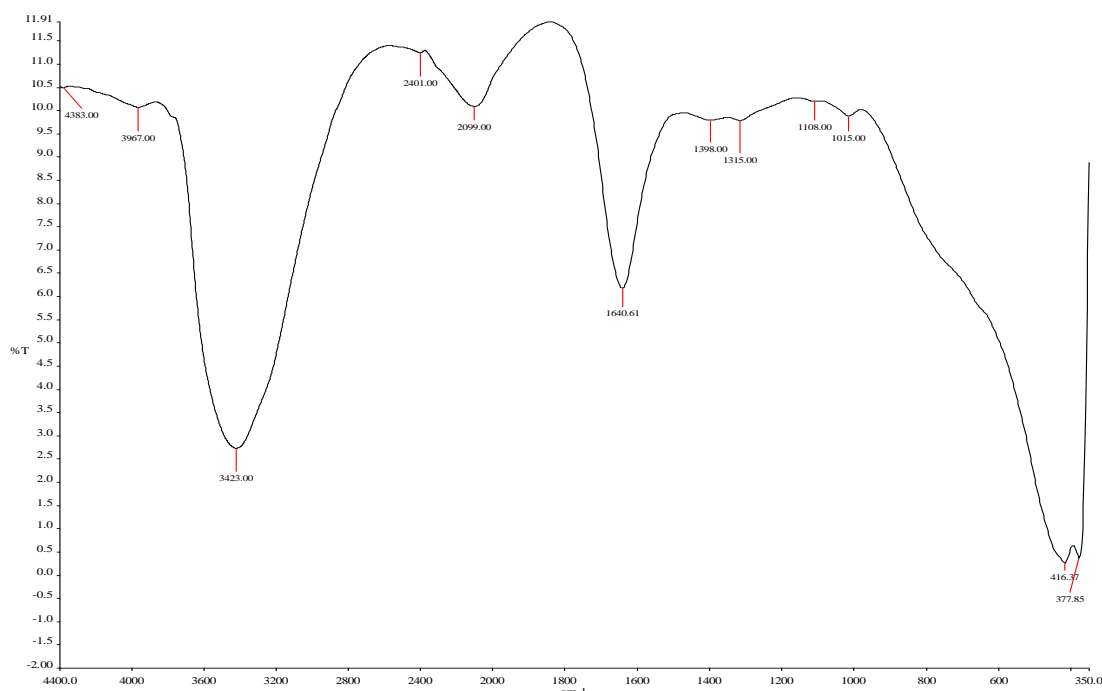


Figure 5: FTIR spectra of activated carbon synthesized using 0.5M of  $\text{ZnCl}_2$

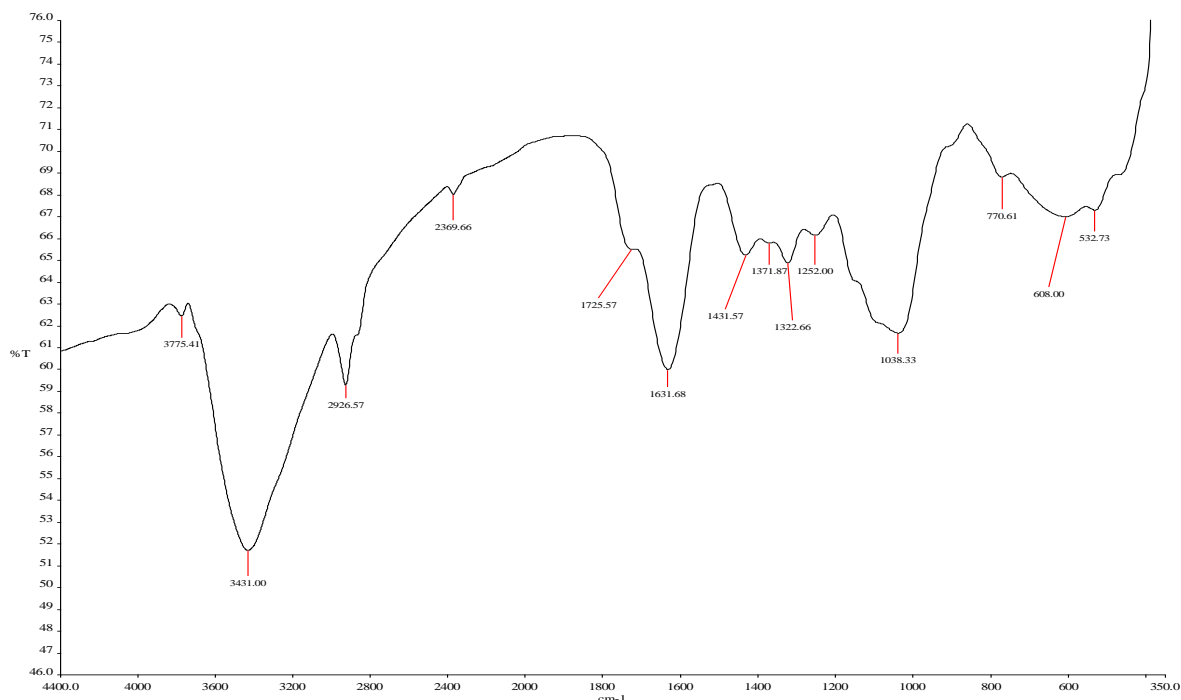


Figure 6: FTIR spectra of activated carbon synthesized using 1.5M of Phosphoric acid

### CONCLUSION

The synthesized activated carbon from watermelon peels were found to have the suitable characteristics of Matrix in the FCCU. Hence, it can be concluded that palm kernel shells and watermelon peels are good starting materials for the production of matrix respectively to be used as a component of the Fluid Catalytic Cracking catalyst.

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